

# Characterization and application of surface-molecular-imprinted-polymer modified TiO<sub>2</sub> nanotubes for removal of perfluorinated chemicals

Lei Hu, Yi Li and Wenlong Zhang

## ABSTRACT

The removal of perfluorinated chemicals (PFCs) during wastewater reclamation is a great concern. However, the existing advanced treatment processes are inefficient for the removal of PFCs from secondary effluents of municipal wastewater treatment plants (WWTPs) because other coexistent pollutants with less environmental significance are removed simultaneously. Therefore, research on high-selectivity, low-cost removal methods is needed. The S-MIP-TiO<sub>2</sub> nanotube (NT) photocatalysts were fabricated, characterized and tested for removal of PFCs from wastewater for the first time. Scanning electron microscopy and Fourier transform infrared spectroscopy show that the TiO<sub>2</sub> NTs (average diameter 60 nm) were successfully imprinted with functional groups (i.e. carboxyl). The adsorption selectivity and photocatalytic activity of the S-MIP-TiO<sub>2</sub> NTs over perfluorooctanoic acid (PFOA) were improved compared with neat TiO<sub>2</sub> NTs and interestingly, were higher at low PFOA concentrations (10 to 100 ng/L, as normal PFC concentrations in secondary effluents) than at high concentrations (10 to 1,000 mg/L). With S-MIP-TiO<sub>2</sub> NTs used as photocatalysts, some representative PFCs were selectively and rapidly removed from secondary effluents of a municipal WWTP. S-MIP-TiO<sub>2</sub> NTs exhibited excellent regeneration performance. Thus, photocatalytic treatment using is promising for effective removal of PFCs from secondary effluents of municipal WWTPs.

**Key words** | perfluorinated chemicals, removal, surface-molecular-imprinting, TiO<sub>2</sub> nanotubes

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## INTRODUCTION

In recent years, wastewater reclamation from municipal wastewater treatment plants (WWTPs) has been employed worldwide for various purposes, including landscape irrigation, impoundment, crop irrigation, and groundwater recharge to overdrawn aquifers (Zhang *et al.* 2011). However, many types of pollutants still exist in the effluents of municipal WWTPs after traditional treatment (Gupta *et al.* 2011b, 2012a). Among them, perfluorinated chemicals (PFCs) are at mean concentrations from ng/L to µg/L. Some PFCs, such as perfluorinated acid, are included in the European Union list of priority pollutants. These chemicals even at trace levels can induce extensive reproductive and sexual abnormalities in wildlife (Radjenovic *et al.* 2007). Thus, the removal of these PFCs during wastewater reclamation is a great concern.

Many methods, such as activated carbon adsorption, ozonation, UV radiation, UV/H<sub>2</sub>O<sub>2</sub> degradation, and

photo-degradation, have been developed to remove PFCs from wastewater (Zhang *et al.* 2012). Among them, activated carbon has been widely applied to remove organic matters from wastewater owing to its strong affinity to adsorb even low-concentration organic substances (Ali & Gupta 2006; Gupta *et al.* 2006, 2007; Gupta & Ali 2008; Gupta *et al.* 2011a). Photo-degradation is an environmentally friendly technique since it does not require chemical input or output (Gupta *et al.* 2007, 2011b, 2012b). TiO<sub>2</sub> is the most common photocatalyst due to its capability in removal of a wide range of pollutants, and shows other advantages including high photochemical stability, low toxicity and low-cost (Gupta *et al.* 2011a, 2012a).

However, the presence of low-level PFCs is accompanied by high levels of other low-toxicity biodegradable pollutants in secondary effluents of municipal WWTPs (Saadi *et al.* 2006). Current advanced treatment processes

are inefficient for PFCs removal because other pollutants with less environmental significance were also removed simultaneously, which decreases the removal efficiency of PFCs and increases treatment costs (Czili & Horvath 2008). For these reasons, the research for highly selective and low-cost removal methods is still warranted.

Molecular imprinting is a useful technique for the preparation of polymeric materials as specific molecular recognition receptors (Piletsky *et al.* 2001; Haupt 2003). Molecularly imprinted polymers (MIPs) are prepared by copolymerization of a cross-linking agent with the complex formed from a template and polymerizable monomers that have functional groups specifically interacting with the template through covalent or non-covalent bonds. After the template is removed from the resulting polymer matrixes, binding sites having the size and shape complementary to the template are generated. These MIPs are synthesized with 'tailor-made' binding sites for a template (Haupt 2003). Recently, MIPs have been utilized for the selective removal of perfluorinated compounds from water (Meng *et al.* 2005; Le Noir *et al.* 2007; Zhang *et al.* 2011). Meng *et al.* (2005) suggested that MIPs with perfluorinated acid as template might be used to remove perfluorinated compounds from water. Le Noir *et al.* (2007) employed MIPs, based on bulk polymerization approach, to remove trace perfluorinated acid from aqueous solution using MIPs adsorbent column. Tran *et al.* (2014) used molecularly imprinted polymeric microspheres to remove phenolic estrogen pollutants from different sources of water. The results of the above studies show that MIPs adsorption is an effective method for the selective removal of trace targeted perfluorinated compounds from water.

However, adsorption is a non-destructive removal technology and MIPs need to be regenerated and reused for a lower treatment cost (Sansotera *et al.* 2014). The related research concerning simultaneous adsorption of perfluorinated compounds and polymer regeneration are very limited. Only recently, UV irradiation was used as a method to regenerate MIPs and destroy pollutants during solvent extraction (Jing *et al.* 2014). It has been reported in our previous research that TiO<sub>2</sub> photocatalysis is more effective for the removal of perfluorinated compounds and perfluorinated activity from secondary effluents than UV irradiation (Zhang *et al.* 2012). However, to the best of our knowledge, there is no existing report regarding the selective removal of perfluorinated compounds using the technology combining of MIPs adsorption and TiO<sub>2</sub> photocatalysis.

The main objective of this work was, therefore, to develop new surface-MIP-modified TiO<sub>2</sub> (S-MIP-TiO<sub>2</sub>) nanotube (NT)

photocatalysts to achieve selective removal of perfluorinated compounds from secondary effluents and simultaneous regeneration of polymers. The material characteristics, adsorption properties, and photocatalytic activity of the photocatalysts were investigated in details. The photocatalytic removal of PFCs and perfluorinated activity from practical secondary effluent using S-MIP-TiO<sub>2</sub> NTs were also evaluated.

## MATERIAL AND METHODS

### Reagents

The titanium sheets (99.60%, 0.06 mm thick) were purchased from Haiji Ltd for Titanium & Nickel, China. The five perfluorinated compounds [heptafluorobutyric acid (PFBA), perfluorovaleric acid (PFPeA), undecafluorohexanoic acid (PFHxA), perfluoroheptanoic acid (PFHpA), and pentadecafluorooctanoic acid (PFOA)], methacrylic acid (MAA), trimethylolpropane trimethacrylate (TRIM), and 4,4'-azobis(4-cyanovaleric acid) (AIBN) were all purchased from Sigma-Aldrich (USA) and used without further purification. TRIM was of technical grade and all other reagents used were of high-performance liquid chromatography (HPLC) grade. Analytical standards for chromatography analyses were purchased from Sigma-Aldrich (USA).

### Preparation of TiO<sub>2</sub> NTs and S-MIP-TiO<sub>2</sub> NTs

TiO<sub>2</sub> NTs were prepared according to previous work (Su *et al.* 2009). Prior to anodization, titanium sheets were ultrasonically cleaned in acetone and deionized water. The cleaned titanium sheet was anodized at 20 V in an electrolyte containing 0.5 wt% NH<sub>4</sub>F and 1/12 M C<sub>2</sub>H<sub>2</sub>O<sub>4</sub>·2H<sub>2</sub>O at room temperature for 10 min in a two-electrode system with a nickel cathode. To induce crystallinity, the initially amorphous as-anodized sample was annealed at 500 °C for 120 min with heating and cooling rates of 2 °C·min<sup>-1</sup>.

The MIP was prepared by precipitation polymerization method. The template (PFOA, 0.18 mmol) was first added into a bottle containing a mixture of solvent (anhydrous acetonitrile, 10 mL) and functional monomer (MAA, 0.87 mmol), and sonicated for 5 min at ambient temperature. The cross-linker (TRIM, 1.90 mmol) and initiator (AIBN, 0.0071 mmol) were then added into the solution. The solution was mixed uniformly by sonication for 5 min, and then was slowly dropped on two sides of TiO<sub>2</sub> NTs to get a uniform coating. Afterwards, the coated-TiO<sub>2</sub> NTs were fixed in the columniform quartz tube. The tube was

then sealed and purged with nitrogen for a further 20 min. Polymerization was carried out under UV light irradiation for 12 h. Then the coated-TiO<sub>2</sub> NTs were washed with a mixture of methanol and acetic acid (volume ratio of 9:1) for four times, and each at a duration of 1.5 h. Then, the nanotube array was washed with methanol for 24 h. This was followed by extractions with methanol until no PFOA was detected in the eluates. The non-imprinted polymer (NIP) modified TiO<sub>2</sub> nanotubes were synthesized and treated in the same way except that no template was added.

### Characterization

The morphological characters of the samples were investigated using field emission scanning electron microscope (Hitachi, Model S-4800). The completion of the reaction in the preparation of the MIPs modified NTs was demonstrated by FD-5DX Fourier transform infrared spectroscopy (FT-IR). The crystal phases were determined by X-ray diffractometer (XRD, M21X, MAC Science Ltd, Japan) with Cu-K<sub>α</sub> radiation.

### Apparatus and methods for adsorption and photocatalytic degradation

The adsorption of PFOA on MIP-TiO<sub>2</sub> NTs, NIP-TiO<sub>2</sub> NTs and TiO<sub>2</sub> NTs were performed by placing these samples in the solutions (300 mL) at different concentrations of PFOA (varied from 10 to 10<sup>9</sup> ng/L). The whole process went on with continuous magnetic stirring for 2 h in the dark at room temperature. The amount of adsorbed PFOA was determined by measuring the difference between total PFOA amount and residual amount in solution.

The photocatalytic experiments were conducted in a water-jacketed cylindrical quartz photocatalytic reactor (60 cm height, 18 cm outer diameter, and 15 cm inner diameter) in the presence of the photocatalysts with the active area 400 cm<sup>2</sup>/L. The double-walled glass reservoir was equipped with a thermostatically controlled water flow between the outer walls. The aeration system at the bottom of the reactor was installed to improve mixing and mass transfer to the catalyst. An 8 W, low-pressure mercury UV lamp (Beijing Lighting Research Institute, ZW8S15W) with irradiating wavelength 254 nm as the light source was immersed in the photocatalytic reactor. Under the same conditions as in the photocatalytic experiments, the total useful radiation arriving to the reactor was determined to be  $7.38 \times 10^{-8}$  Einstein·s<sup>-1</sup> by chemical actinometry using potassium ferrioxalate (Sun & Bolton 1996). After the

solution was stirred for 40 min to favor the organic adsorption onto the catalyst surface, the concentration of the pollutant was determined as the initial concentration, and then the irradiation started. The solution was sampled for analysis from the reactor cell using a glass syringe at specified time intervals during degradation.

### Analytical methods

The concentrations of PFOA in ultrapure water were determined using liquid chromatography–mass spectrometry (LC-MS) equipped with electrospray interface (HP 1100 LC-MS<sub>n</sub> Trap SL System, Agilent, USA) in negative ionization mode for isolation of *m/z* 271 ([M-H]<sup>-</sup> ion). During the process, the mobile-phase composition was methanol/water 75/25 (v/v) at a flow rate of 0.18 mL·min<sup>-1</sup>. Stop time was set to be 6 min.

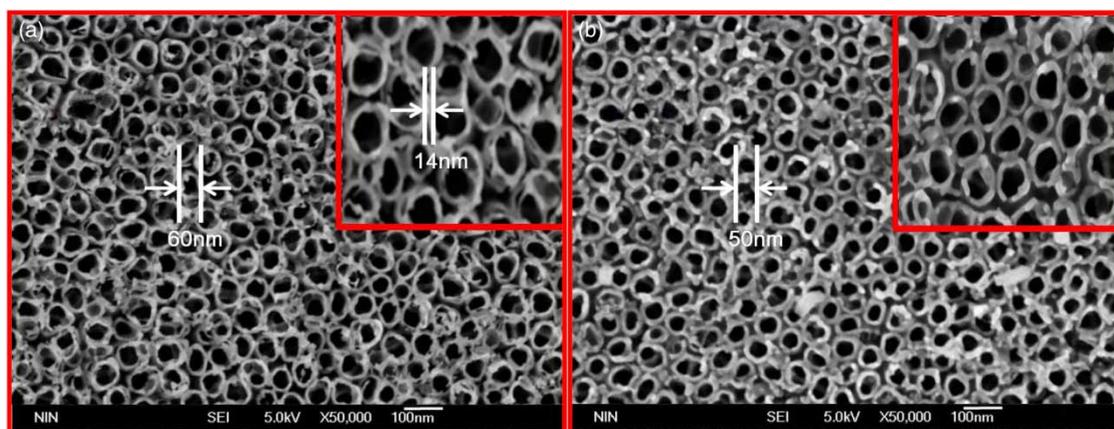
To determine the PFCs in secondary effluents, solid phase extraction (SPE) method was applied to concentrate the compounds from the wastewater sample using Oasis HLB resin cartridges (Waters Corporation, USA) previously washed with 10 mL of ethyl acetate, 10 mL methanol, and 15 mL ultrapure water. The dried eluate post SPE were derived with 100 μL pyridine and 50 μL *N,O*-bis(trimethylsilyl) trifluoroacetamide solution containing 1% trimethylchlorosilane (Sigma) at 70 °C for 60 min, followed by cooling down to room temperature.

## RESULTS AND DISCUSSION

### Characterization of as-prepared photocatalyst

The surface morphologies of TiO<sub>2</sub> NTs and S-MIP-TiO<sub>2</sub> NTs are shown in Figure 1. Neat TiO<sub>2</sub> NTs (Figure 1(a)) were composed of well-ordered and uniform TiO<sub>2</sub> nanotubes, with pore sizes ranging from 55 to 75 nm, and the average pore size of approximately 60 nm, and a wall thickness of approximately 14 nm. Most S-MIP-TiO<sub>2</sub> NTs (Figure 1(b)) were still open at the top end, similar with the TiO<sub>2</sub> NTs. In the process of MIP modification, the mixture was supposed to diffuse down the length of the hollow core of the NTs. Hence, the inside surface of the NTs was modified with a thin MIP layer, decreasing the average diameter from approximately 60 to 50 nm.

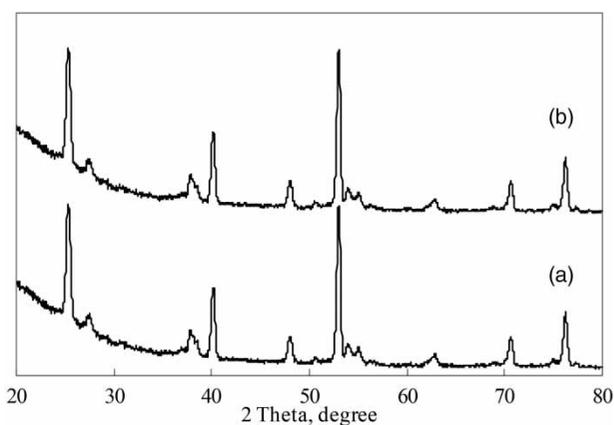
Compared with TiO<sub>2</sub> NTs (Figure 2(a)), the IR spectrum of the TiO<sub>2</sub> NTs with a PFOA-imprinted layer (Figure 2(b)) had the characteristic peaks of PFOA at 3,446, 3,240, 2,930, 2,864, 1,590, and 1,250 cm<sup>-1</sup> (Cakmak *et al.* 2006), and the characteristic peaks of MAA at 1,650 and 1,820 cm<sup>-1</sup>



**Figure 1** | Surface-view SEM images of: (a) TiO<sub>2</sub> NTs, (b) S-MIPs-TiO<sub>2</sub> NTs.

(Martínez *et al.* 2008). After removing PFOA using methanol and acetic acid, the characteristic peaks assigned to PFOA disappeared. In contrast, the characteristic peaks assigned to MAA were still clearly observed (Figure 2(c)). This result indicated that the functional monomer of the target molecule PFOA was successfully imprinted on the surface of TiO<sub>2</sub> NT.

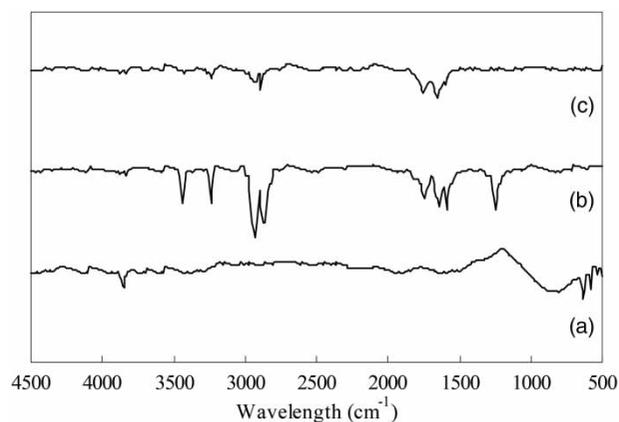
Both the XRD spectra of the neat TiO<sub>2</sub> NTs (Figure 3(a)) and S-MIP-TiO<sub>2</sub> NTs (Figure 3(b)) exhibited clear characteristic diffraction peaks at 25.34°, 37.84°, 48.02°, 53.00°, 55.02°, 62.86°, 70.58°, and 76.24°, which were assigned to the anatase phase. The XRD patterns revealed the crystallization of TiO<sub>2</sub> NTs was not affected by the surface molecular imprinted process.



**Figure 3** | XRD patterns of (a) TiO<sub>2</sub> NTs, (b) S-MIPs-TiO<sub>2</sub> NTs.

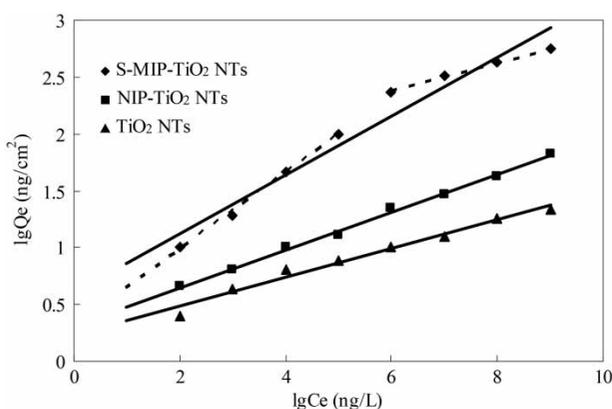
### Adsorption of the template molecules

The adsorption of the template compounds PFOA on S-MIP-TiO<sub>2</sub> NTs, NIP-TiO<sub>2</sub> NTs, and TiO<sub>2</sub> NTs are shown



**Figure 2** | FT-IR spectra of (a) TiO<sub>2</sub> NTs, (b) S-MIPs-TiO<sub>2</sub> NTs before being treated with methanol and acetic acid, (c) S-MIPs-TiO<sub>2</sub> NTs.

in Figure 4. The adsorption isotherms were described by the Freundlich isotherm model ( $Q_e = K_f C_e^{1/n}$ ). In this model,  $Q_e$  is the amount of PFOA adsorbed per unit active surface area of the photocatalysts ( $\text{mg}\cdot\text{cm}^{-2}$ ),  $C_e$  is the concentration of PFOA in solution ( $\text{ng}\cdot\text{L}^{-1}$ ),  $K_f$  is the adsorption equilibrium constant representative of the adsorption capacity, and  $1/n$  is a constant indicative of the adsorption intensity. The values of the parameters are listed in Table 1. In the investigated concentration range,  $1/n$  of the S-MIP-TiO<sub>2</sub> NTs (0.2711) was higher than that of the NIP-TiO<sub>2</sub> NTs (0.1754) and TiO<sub>2</sub> NTs (0.1187).  $K_f$  of the S-MIP-TiO<sub>2</sub> NTs was 3.89, higher than those for NIP-TiO<sub>2</sub> NTs and TiO<sub>2</sub> NTs (2.04 and 1.65, respectively). These results indicated that the adsorption capacity and intensity of both S-MIP-TiO<sub>2</sub> NTs and NIP-TiO<sub>2</sub> NTs were enhanced during the precipitation polymerization process. The S-MIP-TiO<sub>2</sub> NTs had the highest adsorption capacity and intensity among the three photocatalysts.



**Figure 4** | Adsorption isotherms of S-MIP-TiO<sub>2</sub> NTs, NIP-TiO<sub>2</sub> NTs, and TiO<sub>2</sub> NTs for PFOA in ultrapure water.

According to the adsorption isotherms, an adsorption hypothesis involving three types of potential binding sites on the surface of the modified photocatalyst was proposed as shown in Figure 5. For binding site type 1, only the template molecules could be bound theoretically because the binding sites require not only specific functional groups, but also matching target molecule sizes. Binding site type 2 could occur both specific by specific functional group recognition and non-specific adsorption via hydrogen bonding. Binding site type 3 could occur non-specific adsorption via hydrogen bonding. After polymerization, some functional monomers that do not form complexes could remain on the surface of the polymer. These monomers provide the possibility of non-specific adsorption via hydrogen bonding. Three types of potential binding sites could be formed on the surface of S-MIP-TiO<sub>2</sub> NTs, and one type (type 3) on the surface of the NIP-TiO<sub>2</sub> NTs.

In general, the Freundlich model is suitable for assessing the adsorption isotherm of S-MIP-TiO<sub>2</sub> NTs. However, in the current study, the Freundlich model yielded a worse fit for the adsorption isotherm of PFOA on S-MIP-TiO<sub>2</sub> NTs ( $R^2 = 0.9361$ ) than in previous studies ( $R^2 \geq 0.99$ ) (Zhang *et al.* 2008). This discrepancy can be explained by the fact that

the investigated adsorption concentration range (from 10 ng/L to 1,000 mg/L) was much wider than those in previous studies (from 1 to 1,000 mg/L) (Zhang & Hu 2008). The adsorption isotherms of PFOA on S-MIP-TiO<sub>2</sub> NTs are shown in Figure 4. It could be found that the Freundlich model constant  $1/n$  at low concentrations of PFOA (from 10 to 10<sup>5</sup> ng/L) was higher than that at high concentrations (from 10<sup>6</sup> to 10<sup>9</sup> ng/L). It indicated that the adsorption intensity of PFOA on S-MIP-TiO<sub>2</sub> NTs at low concentrations (from 10 to 10<sup>5</sup> ng/L) was higher than that at high concentrations (from 10<sup>6</sup> to 10<sup>9</sup> ng/L). According to the adsorption hypothesis proposed in this study, the adsorption of template compounds on the S-MIP-TiO<sub>2</sub> NTs had two different adsorption mechanisms, i.e. functional group recognition and interaction between  $\pi$  electrons. The attractive force of functional group recognition between carboxyl and phenolic hydroxyl is stronger than the interaction force between  $\pi$  electrons in the phenol aromatic ring and in the cross-linker (Wang *et al.* 2006; An *et al.* 2008; Alizadeh & Akhondian 2010). Therefore, the adsorption of low concentration PFOA on S-MIP-TiO<sub>2</sub> NTs most resulted from functional group recognition (potential binding sites 1 and 2). In contrast, the weak interaction forces (potential binding site 3) were the major adsorption mechanism at high concentrations of PFOA. It can be deduced that the functional group recognition exhibited higher adsorption intensity towards the template molecules than weak interaction.

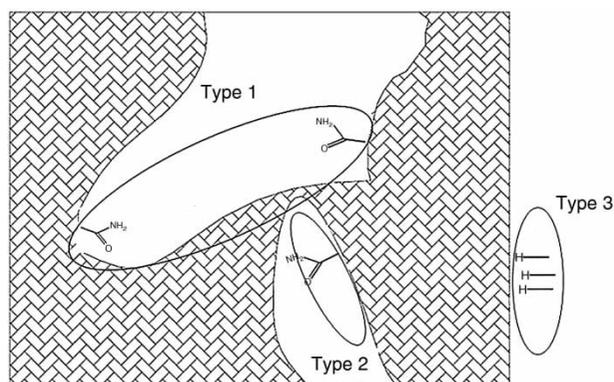
### Photocatalytic removal of the template molecules

The photocatalytic degradation activities of the S-MIP-TiO<sub>2</sub> NTs, NIP-TiO<sub>2</sub> NTs, and TiO<sub>2</sub> NTs were evaluated in an aqueous PFOA solution. The photocatalytic reaction kinetics followed the Langmuir-Hinshelwood model (Zhang *et al.* 2011).

$$r = \frac{dC}{dt} = \frac{kKC}{1 + KC} \quad (1)$$

**Table 1** | Freundlich isotherm parameters for adsorption PFOA

Photocatalysts	Initial concentration (ng/L)						$K_f$
	[10, 10 <sup>5</sup> ]		[10 <sup>6</sup> , 10 <sup>9</sup> ]		[10, 10 <sup>9</sup> ]		
	1/n	$R^2$	1/n	$R^2$	1/n	$R^2$	
S-MIP-TiO <sub>2</sub> NTs	0.3381	0.9969	0.1253	0.9938	0.2711	0.9316	3.89
NIP-TiO <sub>2</sub> NTs	–	–	–	–	0.1754	0.9969	2.04
TiO <sub>2</sub> NTs	–	–	–	–	0.1187	0.9985	1.65



**Figure 5** | Three potential binding sites on the surface of the modified photocatalyst.

where  $C$  is the PFOA concentration,  $k$  is the degradation rate constant, and  $K$  is the adsorption equilibrium constant. In the current study, the PFOA concentration  $C$  was less than  $1 \times 10^{-3} \text{ mol}\cdot\text{L}^{-1}$ , which made  $KC < 1$ . Hence, Equation (1) can be transformed into:

$$r = \frac{dC}{dt} = kKC = k_{app}C \quad (2)$$

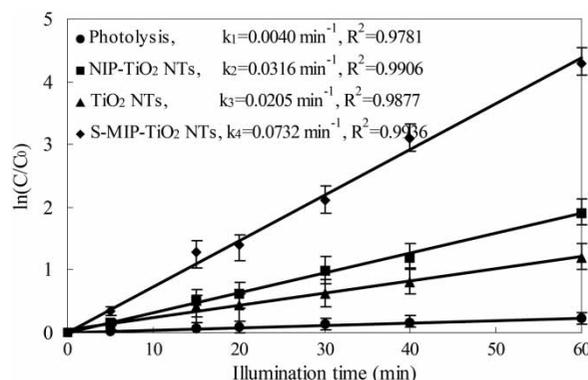
The integration of Equation (2) would lead to the expected relationship:

$$\ln\left(\frac{C_0}{C}\right) = k_{app}t \quad (3)$$

$$k_{app} = kK \quad (4)$$

where  $C_0$  and  $C$  are the concentrations of PFOA at the beginning and at time  $t$ , respectively, and  $k_{app}$  is the apparent degradation rate constant. PFOA degradation in the UV irradiation experiments also followed a pseudo-first-order kinetics (Sansotera et al. 2014). As shown in Figure 6, the apparent first-order rate constant  $k_{app}$  in a different process can be easily calculated:  $0.0040 \text{ min}^{-1}$  in the photolysis process,  $0.0225 \text{ min}^{-1}$  for the  $\text{TiO}_2$  NTs,  $0.0316 \text{ min}^{-1}$  for the NIP- $\text{TiO}_2$  NTs, and  $0.0732$  for the S-MIP- $\text{TiO}_2$  NTs in the photocatalytic process, respectively. These results indicated that  $\text{TiO}_2$  photocatalysis was more efficient than direct photolysis for PFOA removal, and the photocatalytic degradation process was enhanced with the presence of the MIP layer.

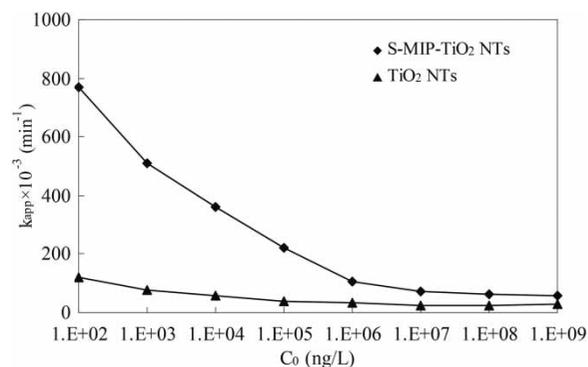
In this process, the photocatalytic reaction started with the adsorption of the template compound molecules PFOA on the MIPs layers located on the surface  $\text{TiO}_2$  NTs. Then the adsorbed PFOA molecules were oxidized by the generated  $\cdot\text{OH}$  radicals during photocatalysis.



**Figure 6** | Kinetic data for direct photolysis and photocatalytic degradation of PFOA over S-MIP- $\text{TiO}_2$  NTs, NIP- $\text{TiO}_2$  NTs, and  $\text{TiO}_2$  NTs. The initial concentration of PFOA was  $10 \mu\text{g/L}$ .

Therefore, the photocatalytic degradation rate strongly depended on the amount of PFOA adsorbed on the photocatalyst surface, and on the amount of  $\cdot\text{OH}$  generated during photocatalysis, as shown in Equation (4). It has been confirmed that the adsorption capacity and intensity of PFOA on S-MIP- $\text{TiO}_2$  NTs was higher than  $\text{TiO}_2$  NTs, although the incident light would be hindered by MIPs layer on the surface of  $\text{TiO}_2$  NTs, and thus hinder the  $\cdot\text{OH}$  generation during S-MIP- $\text{TiO}_2$  photocatalysis (Liu et al. 2010). Therefore, the enhanced photocatalytic degradation should result from the enhanced adsorption capacity and intensity despite the negative effects of MIPs layer.

The effect of concentration on the photocatalytic degradation rate of PFOA was also investigated. As shown in Figure 7, when the initial PFOA concentration increased from  $10^2 \text{ ng/L}$  to  $10^9 \text{ ng/L}$ ,  $k_{app}$  of PFOA degradation decreased from  $0.784$  to  $0.071 \text{ min}^{-1}$  using the S-MIP- $\text{TiO}_2$  NTs, and from  $0.109$  to  $0.029 \text{ min}^{-1}$  using the  $\text{TiO}_2$  NTs. The ratio of the  $k$  values using S-MIP- $\text{TiO}_2$  NTs to  $\text{TiO}_2$  NTs was decreased from 7.19 to 2.45. The result indicated



**Figure 7** | Initial concentration dependence of the degradation rate constant of PFOA over the corresponding S-MIP- $\text{TiO}_2$  NTs and  $\text{TiO}_2$  NTs.

that the degradation selectivity of S-MIP-TiO<sub>2</sub> NTs towards the template compounds (PFOA) was increased as the initial concentration of PFOA was decreased, which would be helpful for the selective removal of the low-level template compounds in wastewater.

Based on the above analysis, the S-MIP-TiO<sub>2</sub> NTs not only exhibited outstanding adsorption capacity and photocatalytic activity toward the template compounds, but also had higher adsorption intensity and photocatalytic selectivity at low concentrations than that at high concentrations. Therefore, photocatalytic treatment using S-MIP-TiO<sub>2</sub> NT as photocatalysts may be a promising approach for the removal of trace perfluorinated compounds from secondary effluents.

### Photocatalytic removal of PFCs

The feasibility of applying S-MIP-TiO<sub>2</sub> NTs for the selective removal of perfluorinated compounds from wastewater was evaluated by investigating the photocatalytic removal efficiency of five perfluorinated compounds (PFBA, PFPeA, PFOA, PFHxA, and PFHpA) from the secondary effluents of a municipal WWTP as shown in Figure 8. The initial concentration of five PFCs was 10 µg/L. These compounds were chosen as the representative chemicals to be detected in the secondary effluents because of their wide occurrence and high potential toxicity.

It is known that the photocatalytic degradation process can be divided into two stages, i.e. adsorption and photocatalytic degradation phases. In adsorption phase (0–40 min), the functional group recognition was the major adsorption mechanism because the concentrations of PFCs in secondary effluent range from ng/L to µg/L. As shown in previous work, the functional group recognition is the chemical interaction between the functional groups (–OH)

in target molecules and the footprints groups (carboxyl) in polymer. Therefore, the compounds comprising the functional groups in their molecules (such as PFBA, PFPeA, PFHxA, and PFHpA) were chemically adsorbed on the surface of S-MIP-TiO<sub>2</sub> NTs, resulting in an enhanced photocatalytic degradation and a rapid removal of PFCs. In comparison, the compounds without these functional groups were not enhanced adsorbed and degraded during the same process.

The pH value of the solution is an important parameter, which affects the adsorption behavior of the ion in many cases. The adsorbent surface was charged through the protonation of functional groups and the electrostatic attraction between adsorbents and adsorbates usually plays a major role. It can be found that the adsorption is pH dependent, and the adsorption amount of PFOA decreased with increasing solution pH value. Therefore, the electrostatic interaction played an important role in the sorption process at acidic pH values. With increasing solution pH, the adsorption amount of the MIPs and NIPs adsorbents for PFOA decreased. It indicated that the adsorption of PFOA onto the MIPs and NIPs adsorbents was mainly attributed to the electrostatic attraction. Other forces including hydrophobic interaction and hydrogen binding may be involved in the adsorption in the whole pH range, but their contributions are limited in this study. It also can be found that the MIPs adsorbents had higher sorption capacity than that of the NIPs adsorbents at pH values from 4 to 6, showing the good selective adsorption. The initial pH value of the solution is 5 in this work.

The S-MIP-TiO<sub>2</sub> NTs were also reused to test its stability for the removal of perfluorinated activity from the secondary effluents. It was found that the removal efficiency was slightly reduced after each use and finally stable at about 82% after five cycles. The result indicates that photocatalytic treatment using S-MIP-TiO<sub>2</sub> NTs could be a promising approach for effectively eliminating PFCs from secondary effluents of municipal WWTPs.

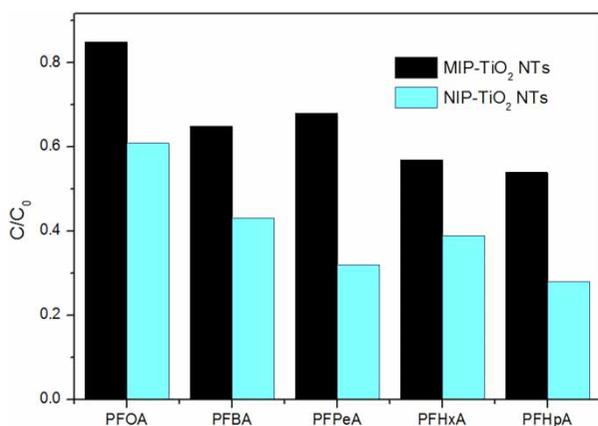


Figure 8 | The removal efficiency of five kinds PFCs.

### CONCLUSIONS

Surface-molecular-imprinted polymer-modified TiO<sub>2</sub> nanotube (S-MIP-TiO<sub>2</sub> NT) photocatalysts were prepared. The MIP layer provided the neat TiO<sub>2</sub> NTs with selective molecular adsorption ability, leading to outstanding adsorption capacity and intensity and enhanced photocatalytic selectivity and activity over PFOA. Moreover, the modified photocatalysts exhibit higher adsorption intensity and

photocatalytic selectivity at low concentrations than at high concentrations.

The photocatalytic removal of PFCs and perfluorinated activity from secondary effluents of a municipal WWTP was considerably enhanced using S-MIP-TiO<sub>2</sub> NTs than using TiO<sub>2</sub> NTs. The S-MIP-TiO<sub>2</sub> NTs developed here also exhibit excellent regeneration performance. Therefore, photocatalytic treatment with S-MIP-TiO<sub>2</sub> NTs could be a promising approach for effective elimination of PFCs from secondary effluents of municipal WWTPs. This method would help to reduce ecological risk during wastewater reclamation.

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